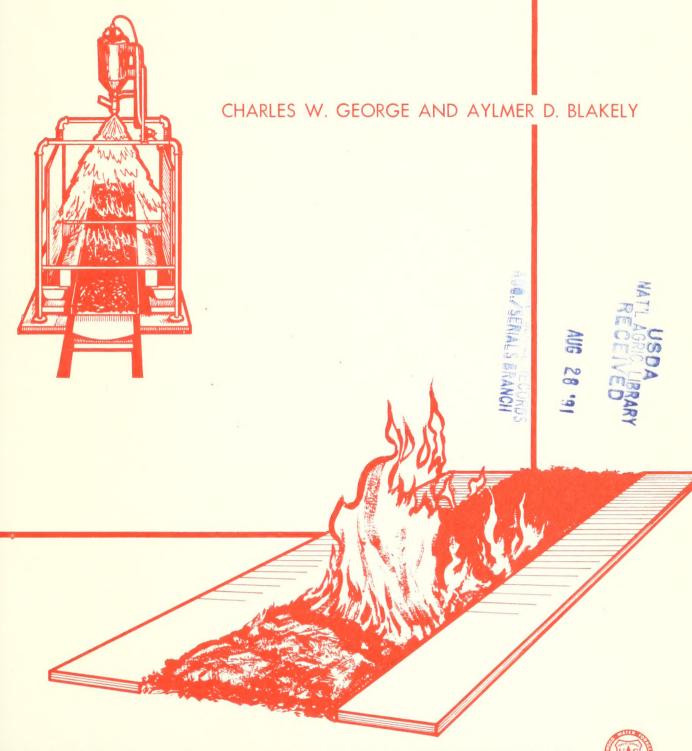
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# Effects Of Ammonium Sulfate And Ammonium Phosphate On Flammability



USDA FOREST SERVICE RESEARCH PAPER INT-121 1972 INTERMOUNTAIN FOREST AND RANGE EXPERIMENT STATION OGDEN, UTAH 84401

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USDA Forest Service Research Paper INT-121 April 1972

# Effects Of Ammonium Sulfate And Ammonium Phosphate On Flammability

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### CONTENTS

| INTRODUCTION                                      | 1 |
|---|---|
| The Problem                                       | 1 |
| Objectives  | 2 |
| THE METHOD  | 3 |
| Type of Fuel and Fuel Bed Configuration           | 3 |
| Method of Chemical Application                    | 4 |
| Conditioning of Fuel and Environmental Conditions | 5 |
| BURNING TEST                                      | 7 |
| Burning Procedures                                | 7 |
| Measurements                                      | 8 |
| RESULTS 10  | 0 |
| DISCUSSION  | 8 |
| LITERATURE CITED                                  | 0 |
| APPENDIX 21                                       | 1 |

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#### ABSTRACT

Ponderosa pine needle and aspen excelsior fuel beds, chosen because they exhibit different chemical fuel characteristics, were treated with various amounts of ammonium sulfate and ammonium phosphate and burned in a wind tunnel under controlled environmental conditions. The rate of fire spread, rate of weight loss (equivalent energy release rate), and the residue were measured to quantify the retardants' effects on flammability.

An increase in the amount of either fire retardant chemical caused a reduction in rate of fire spread and rate of weight loss while increasing the amount of residue. However, at all treatment levels, ammonium phosphate was more effective than ammonium sulfate. These two chemicals exhibit their primary difference in their effect on glowing combustion. The rate of weight loss and especially the residue are parameters that quantify glowing combustion.

Ammonium phosphate is much more effective in decreasing the rate of weight loss and increasing the residue than is ammonium sulfate, which has little effect on the residue. The superior effectiveness of ammonium phosphate is probably due to the difference in thermal behavior of the two fire retardants; total decomposition of ammonium sulfate occurs prior to  $450^{\circ}$  C., about  $250^{\circ}$  C. sooner than ammonium phosphate. Temperatures at the surface of the fuel bed probably are within the range of these total decomposition temperatures. Although ammonium sulfate is effective in retarding flaming combustion, the majority of the chemical may decompose prior to the glowing phase and thus not be available to alter reactions taking place during glowing combustion.

The study provides general relationships which can serve as standards for comparing the effects of other basic chemicals or forest fire retardant additives.

### INTRODUCTION

#### **The Problem**

More than 80 million gallons of fire retardant have been used in the control of forest and rangeland fires by fire control agencies throughout the United States in the last 10 years. These fire retardants are specially formulated and usually contain: an active retardant chemical; coloring agent; corrosion inhibitor; thickening agent; and spoilage inhibitor, when necessary.

The most commonly used active retardant chemicals are ammonium sulfate  $(NH_4)_2SO_4$ and ammonium phosphate  $(NH_4)_2HPO_4$ . These chemicals, when applied to cellulosic fuels, alter the combustion process to produce less flammable products while increasing the amount of nonflammable products. The most efficient use of these chemicals can only be made after thorough quantification of their effects on flammability.

Flammability has been defined as the interaction of ignitibility, sustainability, and combustibility (Anderson 1970). Ignitibility is the ease with which a fuel will ignite. Under given conditions, the most ignitible fuel will ignite with the least energy input. Sustainability is a measure of how well the fuel will continue to burn with or without the heat source after ignition. Combustibility is a measure of the rapidity with which energy is released from the fuel following ignition.

Fire retardant chemicals are often applied to reduce the overall flammability of fuels. In other instances these chemicals are used specifically to reduce the sustainability or combustibility. It is often thought that ignitibility is decreased by treating fuel with retardant chemicals such as ammonium sulfate and ammonium phosphate; however, recent empirical data indicate the reverse--i.e., less energy is necessary for ignition of treated fuel.<sup>1</sup> This fact is substantiated by more sophisticated thermal analysis data which indicate that treated cellulose undergoes pyrolysis and combustion at lower temperatures and with less energy inputs than does untreated cellulose (George and Susott 1971). (Pyrolysis is the thermal degradation of a material.)

<sup>&</sup>lt;sup>1</sup>Unpublished experimental data on file at the Northern Forest Fire Laboratory, USDA Forest Service, Missoula, Montana.

A study of the effects that ammonium sulfate and ammonium phosphate have on flammability must include quantification of several appropriate parameters. Many researchers have used rate of fire spread to assist in the evaluation of fire retardants (Hardy, Rothermel, and Davis 1962; Rothermel and Hardy 1965; Johansen 1967; Eickner and Schaffer 1967). The rate of spread is a measure of sustainability, or the ability of a fire to propagate itself. The combustibility, or rate at which energy is released from the fire. can be measured by monitoring the weight loss rate that occurs during the fire (Rothermel and Hardy 1965; Rothermel and Anderson 1966). Only recently has it been pointed out that retardant chemicals applied to open fuel bed fires may have similar effects on the rate of spread but different effects on the rate of energy release (George and Blakely 1970). Because fire retardants are used to reduce fire spread and combustion rate, it is necessary for both parameters to be quantified.

Although ignitibility and sustainability may be encompassed in rate of spread measurements, and combustibility in energy-release rate measurements, they do not entirely describe a fire retardant's effect on flammability. Combustion can be divided into two phases: flaming (associated mainly with the fire front); and glowing (associated with residual burning)--different rates of energy release apply for each of these. The retardant chemical, due to inherent decomposition characteristics, may only be available at given temperatures or for a given time during the fire, (George and Susott 1971) thus causing different effects on the flaming and glowing processes. The extent of combustion, both flaming and glowing, can be determined by measuring the amount of residue.

The quantification of the effects that fire retardants have on rate of spread, energy release rates, and residue should provide a basis for determining the chemical's overall effect on flammability.

#### **Objectives**

The major objective of this study was to determine the effects of ammonium sulfate and ammonium phosphate on the flammability of cellulosic fuels. The overall effects on flammability can be characterized by quantification of these effects on the following parameters:

- Rate of spread (R)
   Rate of weight loss (R<sub>y</sub>)
- 3. Residue (R)

Standard curves were developed in this study for each parameter as a function of the amount of retardant chemical applied to the fuel.

The study was designed to provide general information which can be used to evaluate formulated ammonium sulfate and ammonium phosphate fire retardants. The curves will be used to evaluate the relative importance of additives, or impurities, and to determine whether they enhance or reduce the active chemicals' effectiveness. This information will be useful to potential suppliers for the formulation of more efficient fire retardants.

Also, this study will provide information which may eventually be used in the development of operational guidelines. The guidelines could assist fire control personnel in selecting the most efficient retardant chemical for a given job and help determine how much chemical is required for the specific situation.

# THE METHOD

The development of a method to evaluate the effect of retardant chemicals on flammability required considerable attention to the following:

1. Type of fuel and fuel bed configuration;

2. Method of chemical application; and

3. Conditioning of fuel following chemical application and environmental conditions during burning.

#### **Type of Fuel and Fuel Bed Configuration**

Previous research on the effects of fire retardants (Hardy, Rothermel, and Davis 1962; Rothermel and Hardy 1965) demonstrated the usefulness of ponderosa pine needle fuel beds which were originally used because of their natural physical and chemical characteristics; whether or not this type of fuel is representative of most forest fuel was questioned.

Ponderosa pine needles alone are not representative because they contain a relatively high amount of ether extractives (approximately 10 percent) which apparently volatilize at low temperatures and support combustion. Furthermore, woody fuels make up a large portion of natural forest fuel and generally contain less extractives and a larger percentage of cellulose. Aspen excelsior (0.021 inch by 0.021 inch by 3 inches), is a representative woody fuel and also exhibits a high degree of reproducibility; thus, it has been used to successfully evaluate fire retardants (USDA Forest Service 1970; USDA Forest Service 1969). This excelsior contains less than 1 percent ether extractives but has nearly the same heat content as ponderosa pine needles. (A comparison of chemical characteristics is given in table 1.) By using both of these fuels the researcher was able to simulate the extremes of chemical fuel characteristics normally found in forest areas.

| Item                                  | : | Aspen<br>excelsior | Ponderosa pine<br>needles |
|---------------------------------------|---|--------------------|---------------------------|
| Cellulose (percent dry weight)        |   | 42.0               | 18.0                      |
| Ash content (percent dry weight)      |   | 0.36               | 3.87                      |
| Silica-free ash (percent dry weight)  |   | 0.36               | 1.55                      |
| ther extractives (percent dry weight) |   | <1.0               | 9.73                      |
| Heat content (B.t.u./1b.)             |   | 8,485              | 8,753                     |

Table 1.--Comparison of chemical characteristics of ponderosa pine needles and aspen excelsior

Ponderosa pine needles for fuel beds were collected and cleaned during the year prior to the tests. The needles were stored indoors until an equilibrium moisture content was reached, and aspen excelsior which had been cut to specifications was given similar treatment. Following this ambient indoor conditioning, moisture contents were between 5 and 8.5 percent (percent of ovendry weight) for both types of fuel.

Fuel beds, fuel bed configuration, and a method of preparation similar to that used by Rothermel and Hardy (1965) was adopted for use in the study. A lighter fuel loading was necessary for aspen excelsior because of its higher surface area-to-volume ratio. Characteristics of the fuel bed are shown in table 2.

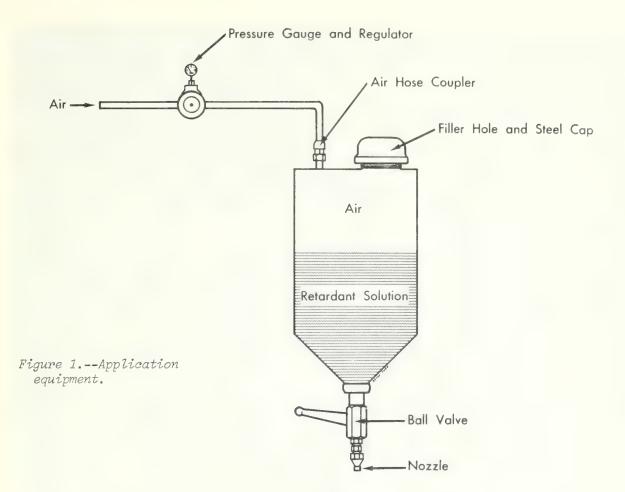
#### **Method of Chemical Application**

A method of application was developed and used to distribute the retardant solution uniformly over the surface of the fuel bed at a constant depth of penetration. This was accomplished by applying a constant volume of solution and varying only the concentration or amount of the chemical in solution. The solution was contained in a pressurized supply tank that had a calibrated flow. The calibration was established by

| Fuel bed (Inches)                           | Average equilibrium :<br>moisture content : | Loading    | at EMC               |                                      | : Fuel bed void<br>: volume-to-surface-<br>: to-area ratio |
|---|---|------------|----------------------|--------------------------------------|--|
|   | Percent                                     | Lb./bed    | Lb./ft. <sup>2</sup> | σ ft. <sup>2</sup> /ft. <sup>3</sup> | $\lambda$ ft <sup>3</sup> /ft <sup>2</sup>                 |
| Aspen excelsior                             |   |            |                      |                                      |  |
| 3 by 18 by 36 <sup>1</sup><br>3 by 18 by 96 | 7.0<br>7.0                                  | 1.5<br>4.0 | 0.33                 | 1,848<br>1,848                       | 9.36 by 10 <sup>-3</sup><br>9.36 by 10 <sup>-3</sup>       |
| Ponderosa pine needles                      |   |            |                      |                                      |  |
| 3 by 18 by 36 <sup>1</sup><br>3 by 18 by 96 | 7.5<br>7.5                                  | 2.25       | .50<br>.50           | 1,741<br>1,741                       | 8.46 by 10 <sup>-3</sup><br>8.46 by 10 <sup>-3</sup>       |

Table 2.--Fuel bed characteristics

<sup>1</sup>Igniter tray.



determining the volume rate through the nozzle at a given pressure while measuring the lateral spray pattern. A nozzle diameter, height, and tank pressure were selected that would provide a uniform lateral pattern over the fuel bed width. The fuel beds were then pushed under the nozzle at a constant predetermined speed to apply the desired amount of solution. The application equipment and spray system in operation are shown in figures 1 and 2.

The fuel beds were weighed prior to and following application of the retardant solution. The amount of solution per square foot of fuel bed and the percent of solution as a function of dry fuel weight were calculated.

#### **Conditioning of Fuel and Environmental Conditions**

Following application of the retardant solution, the fuel beds were allowed to reach an equilibrium moisture content in the combustion chamber under controlled environmental conditions. The combustion chamber air temperature was held at  $90^{\circ} \pm 2^{\circ}$  F. and the relative humidity at  $20 \pm 2$  percent. A new equilibrium moisture content of between 5.0 and 6.5 percent was reached. Equilibrium was determined by periodic weight checks of the fuel bed, and the moisture content was determined by using the xylene distillation method.

All burning tests were made in a large wind tunnel at an air velocity of 5 m.p.h. Fuel bed conditioning and the burning tests were conducted under similar temperature and relative humidity conditions. These conditions are equivalent to a Fine Fuel Spread Index of 36 (USDA Forest Service 1964).



Figure 2 .-- Spray system in operation.

# **BURNING TEST**

#### **Burning Procedures**

Treated and conditioned fuel beds were removed from the combustion chamber and placed on the weighing system in the wind tunnel. The weighing system, described by George and Blakely (1970), was a multiple point system capable of monitoring a weight loss from 0 to 6 pounds, depending on the fuel type and loading; sensitivity of the system was about  $\pm 0.25$  percent, or  $\pm 0.001$  pound. The weighing system utilized transducer-type elements and load cells manufactured by the Statham Instrument Company. The signal from these transducers was summed and averaged to produce a single direct measurable output and then recorded.

Aprons were placed on all sides of the treated fuel beds and the starter beds to produce uniform airflow over the fuel surfaces. A small tray of ethanol (approximately 25 ml.) at the bottom edge of the igniter tray gave uniform ignition at the leading edge. Just prior to test time, a remote controlled electric spark was produced to ignite the ethanol. The positioning of the beds and a schematic of the weighing system are shown in figure 3. The positioning of side aprons and fuel beds during burning is shown in figure 4.

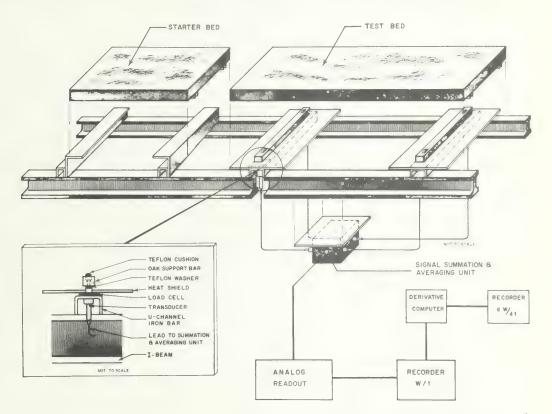


Figure 3.--Multiple strain gage transducer-type weighing system and positioning of starter and treated fuel beds.

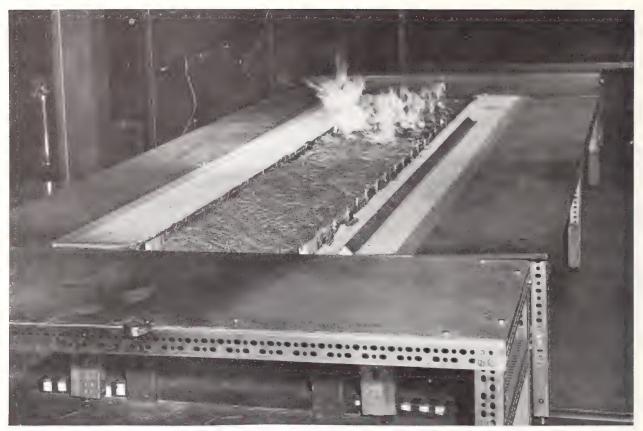


Figure 4. -- Positioning of fuel beds and side aprons during test fire.

#### Measurements

Rate of Spread

The rate at which fire spread through the fuel was measured visually. An aluminum strip with marks at each half-foot interval lay alongside the treated bed. An observer, with a remote switch, activated an event marker which was attached to a recorder being used to record weight loss. The time required for the fire front to cover each half-foot interval was measured and the average steady-state rate of spread between the 3-and 7-foot mark calculated.

#### Weight Loss Rate

The weight of the treated fuel bed was monitored during the fire on a recorder which had previously been calibrated for a full scale deflection of 4.4 pounds (2,000 grams). The weight loss at the 3- and 7-foot intervals was determined. The time between these intervals was computed from the rate-of-spread event marks and then the steady-state rate of weight loss was calculated.

#### Residue

The fuel was allowed to burn until glowing combustion was completed; then the fuel bed was weighed and the residue determined.

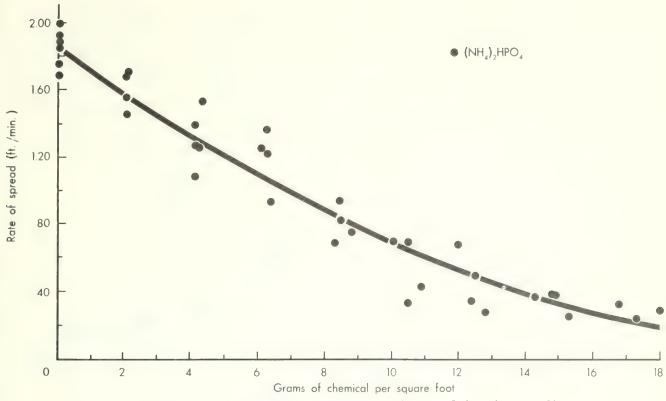
Figure 5 shows a burning test in progress and the equipment being used for taking the required measurements.

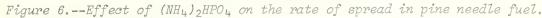


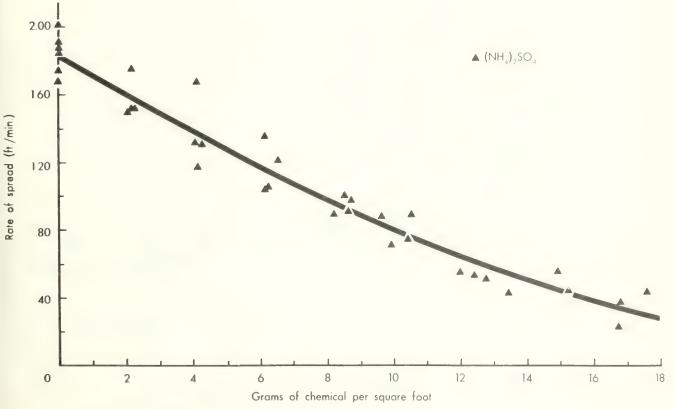
# RESULTS

A total of 133 treated and untreated fuel beds were burned during the study. Of these, 73 were composed of ponderosa pine needles and the remaining were aspen excelsior. The treated beds received applications of  $(NH_4)_2SO_4$  or  $(NH_4)_2HPO_4$ . Data for the untreated fuel beds are given in table 4 of the appendix. A summary of the test data for  $(NH_4)_2HPO_4$  and  $(NH_4)_2SO_4$  treated ponderosa pine needle fuel beds is presented in tables 5 and 6 of the appendix. A summary of the test data for treated aspen excelsior fuel beds is given in tables 7 and 8 of the appendix.

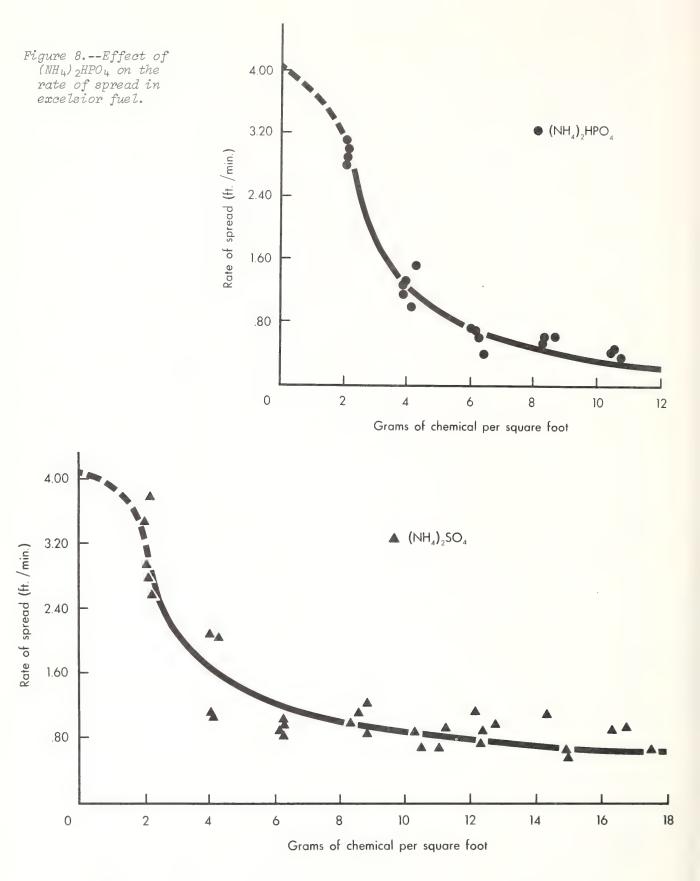
The relationship between the amount of chemical applied per square foot of fuel bed and the rate of fire spread through the pine needle and excelsior fuel beds is shown in figures 6, 7, 8, and 9. The rate of weight loss and equivalent energy release rate (assuming the energy released is equal to heat content of the fuel times the weight loss rate) as a function of the amount of chemical for the two types of fuel beds are shown in figures 10, 11, and 12. The percent increase in residue over the average residue for untreated was calculated for each fire. This percent increase in residue as related to the amount of chemical applied is shown in figures 13 and 14.











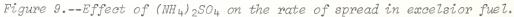
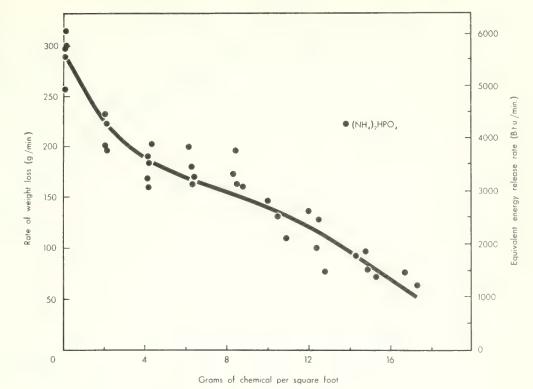


Figure 10.--Effect of (NH<sub>4</sub>)<sub>2</sub>HPO<sub>4</sub> on the rate of weight loss or equivalent energy release rate in pine needle fuel.



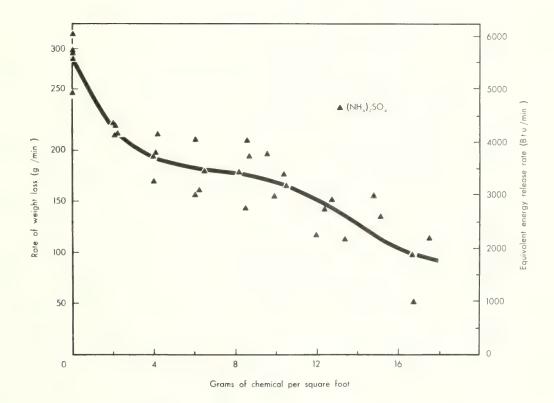


Figure 11.--Effect of  $(NH_4)_2SO_4$  on the rate of weight loss or equivalent energy release rate in pine needle fuel.

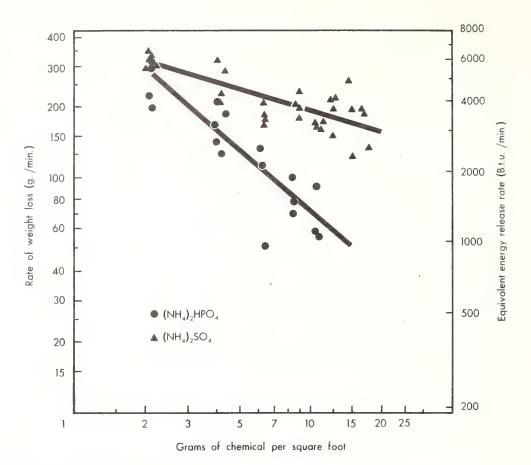
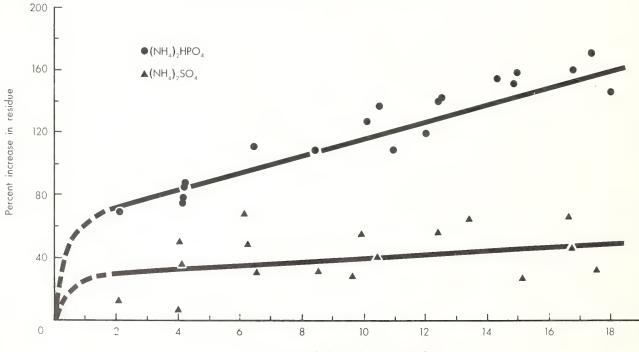


Figure 12.--Effect of  $(NH_4)_2HPO_4$  and  $(NH_4)_2SO_4$  on the rate of weight loss or equivalent energy release rate in excelsior fuel.



Grams of chemical per square foot

Figure 13.--Effect of  $(NH_4)_2HPO_4$  and  $(NH_4)_2SO_4$  on the residue in pine needle fuel.

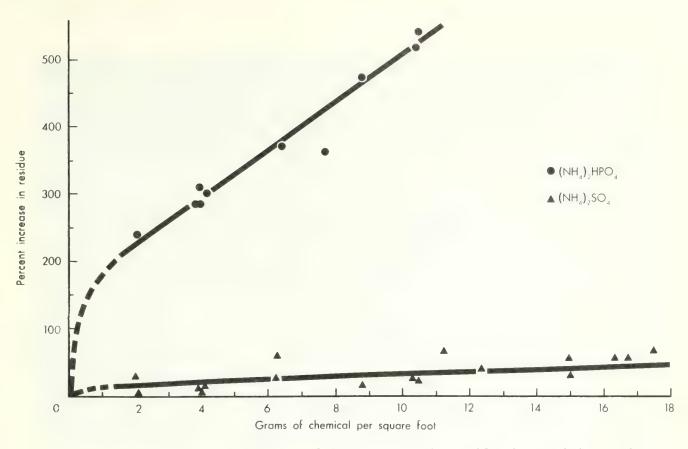


Figure 14.--Effect of  $(NH_{4})_{2}HPO_{4}$  and  $(NH_{4})_{2}SO_{4}$  on the residue in excelsior fuel.

Regression equations were determined for each relationship. The data for both chemical treatments of the same fuel type were then pooled and an analysis of covariance completed. A measure of how well each regression equation fits the sample data is shown by the coefficient of determination,  $r^2$ . The  $r^2$  for each relationship and the  $r^2$  and the F (variance ratio) for the pooled data are given in table 3.

The statistical data indicate that for all parameters measured and for both ponderosa pine needle and aspen excelsior fuel, ammonium phosphate and ammonium sulfate have significantly different effects. The rate of spread in pine needles as a function of the amount of chemical, for both treatments, was the only dependent variable that was not significantly different at the 99 percent level (see table 3).

The regression equations in table 3 (also appendix tables 4 through 8) show that ammonium phosphate reduces the rate of fire spread and rate of weight loss (or equivalent energy release rate) to a greater degree than ammonium sulfate in both the excelsior and pine needle fuel beds. Ammonium phosphate also caused a greater increase in residue, thus decreasing the total energy released.

Ammonium phosphate is more effective than ammonium sulfate in reducing all parameters measured in the study; the largest difference occurs in the greater ability of ammonium phosphate to decrease the rate of weight loss or energy release rate and increase the amount of char or residue formed. Residue in pine needle fuel beds treated with ammonium phosphate showed an 80 to 160 percent increase over residue formed in untreated beds. Ammonium sulfate used under the same conditions did not increase the amount of residue beyond 50 percent. Excelsior fuel beds treated with ammonium phosphate showed an increase in residue of 200 to 500 percent, depending on the treatment level; ammonium sulfate increased the residue only about 50 percent. Figures 15 and 16 show the effects of ammonium sulfate and ammonium phosphate on the residue of combustion occurring in ponderosa pine needle and aspen excelsior fuel beds.

| Ponderoes pine needlesRate of spread (R_s) $(NH_4)_{c}HPO_4$ (DAP44Rate of spread (R_s) $(NH_4)_{c}SO_4$ (AS)41Rate of weight loss (R_w)Pooled85Rate of weight loss (R_w) $(NH_4)_{c}SO_4$ (AS)43Rate of weight loss (R_w) $(NH_4)_{c}SO_4$ (AS)43Rate of weight loss (R_w) $(NH_4)_{c}SO_4$ (AS)43Rate of weight loss (R_w) $(NH_4)_{c}SO_4$ (AS)43Residue (R)Pooled83Residue (R) $(NH_4)_{c}SO_4$ (AS)13Residue (R) $(NH_4)_{c}SO_4$ (AS)14Residue (R)Residue (R)Residue (R)14Residue (R)Residue (R)Residue (R)14 | マ ち ち ち ち ち ち ち ち ち ち ち ち ち ち ち ち ち ち ち                                    | $ = 1.83 - 0.145(x) + 0.00289(x^{2}) $ $ = 1.81 - 0.119(x) + 0.00284(x^{2}) $ $ = 1.82 - 0.131(x) + 0.00234(x^{2}) $ $ = 292 - 43.7(x) + 5.98(x^{2}) - 0.399(x^{3}) + 0.00883(x^{4}) $ $ = 294 - 48.7(x) + 8.05(x^{2}) - 0.583(x^{3}) + 0.0140(x^{4}) $ $ = 294 - 43.3(x) + 6.05(x^{2}) - 0.394(x^{3}) + 0.00848(x^{4}) $ $ = 292 - 43.3(x) + 6.05(x^{2}) - 0.394(x^{3}) + 0.00848(x^{4}) $ $ = 60.4 + 6.06(x) $ $ = 60.4 + 1.18(x) $ $ = 60.4 + 1.18(x) $ $ = 29.5 + 1.18(x) $ | .95<br>.96<br>.91<br>.91                       | 3.15 (f = 3, 79)<br>4.13 (f = 5, 73) | <b>9</b> 0<br>n 0 |
|---|--|---|--|--------------------------------------|-------------------|
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| (NH4,)2SO4 (AS)<br>Pooled<br>(NH4,)2HPO4 (DAP)<br>(NH4,)2SO4 (AS)<br>Pooled<br>(NH4,)2HPO4 (DAP)<br>(NH4,)2SO4 (AS)<br>Pooled   | ママンクロ  | $\begin{array}{l} 0.119(x) + 0.00184(x^{2}) \\ \cdot 0.131(x) + 0.00234(x^{2}) \\ 43.7(x) + 5.98(x^{2}) - 0.399(x^{3}) + 0.00883(x^{4}) \\ 48.7(x) + 8.05(x^{2}) - 0.583(x^{3}) + 0.0140(x^{4}) \\ 43.5(x) + 6.05(x^{2}) - 0.394(x^{3}) + 0.00348(x^{4}) \\ 43.5(x) + 6.05(x^{2}) - 0.394(x^{3}) + 0.00348(x^{4}) \\ \cdot 1.18(x) \\ \cdot 1.18(x) \end{array}$  | .96<br>.91<br>.91<br>.91                       | (f = 3,<br>(f = 5,                   | 50 O              |
| Pooled<br>(NH4)2HPO4 (DAP)<br>(NH4)2SO4 (AS)<br>Pooled<br>(NH4)2HPO4 (DAP)<br>(NH4)2SO4 (AS)<br>Pooled  | マ マ マ マ マ マ マ マ マ マ マ マ マ マ マ マ マ マ マ                                      | <ul> <li>0.131(x) + 0.00234(x<sup>2</sup>)</li> <li>43.7(x) + 5.98(x<sup>2</sup>) - 0.399(x<sup>3</sup>) + 0.00883(x<sup>4</sup>)</li> <li>48.7(x) + 8.05(x<sup>2</sup>) - 0.583(x<sup>3</sup>) + 0.0140(x<sup>4</sup>)</li> <li>43.3(x) + 6.05(x<sup>2</sup>) - 0.394(x<sup>3</sup>) + 0.00948(x<sup>4</sup>)</li> <li>43.3(x) + 6.05(x<sup>2</sup>) - 0.394(x<sup>3</sup>) + 0.00948(x<sup>4</sup>)</li> <li>1.118(x)</li> <li>1.118(x)</li> <li>4.4.43(x)</li> </ul>         | 60° 64 60° 60° 60° 60° 60° 60° 60° 60° 60° 60° | (f = 3,<br>f = 5,                    | 0 0<br>ci 0       |
| (NH4)2HPO4 (DAP)<br>(NH4)2SO4 (AS)<br>Pooled<br>(NH4)2HPO4 (DAP)<br>(NH4)2SO4 (AS)<br>Pooled  | マママン   | $\begin{aligned} &43.7(\mathbf{x}) + 5.98(\mathbf{x}^2) - 0.399(\mathbf{x}^3) + 0.00883(\mathbf{x}^4) \\ &48.7(\mathbf{x}) + 8.05(\mathbf{x}^2) - 0.583(\mathbf{x}^3) + 0.0140(\mathbf{x}^4) \\ &43.3(\mathbf{x}) + 6.05(\mathbf{x}^2) - 0.394(\mathbf{x}^3) + 0.00948(\mathbf{x}^4) \\ &\cdot 1.18(\mathbf{x}) \\ &\cdot 1.18(\mathbf{x}) \end{aligned}$   | 40.<br>10.<br>10.<br>11.                       | ۱                                    | 0)<br>6)          |
| (NH4,)2HPO4 (DAF)<br>(NH4,)2SO4 (AS)<br>Pooled<br>(NH4)2HPO4 (DAP)<br>(NH4,)2SO4 (AS)<br>Pooled   | マック マック  | <pre>43.7(x) + 5.98(x<sup>3</sup>) - 0.399(x<sup>3</sup>) + 0.00883(x<sup>4</sup>)<br/>48.7(x) + 8.05(x<sup>3</sup>) - 0.583(x<sup>3</sup>) + 0.0140(x<sup>4</sup>)<br/>43.3(x) + 6.05(x<sup>3</sup>) - 0.394(x<sup>3</sup>) + 0.00948(x<sup>4</sup>)<br/>43.118(x)<br/>+ 1.18(x)<br/>+ 4.43(x)</pre>   | .94<br>.91<br>.91<br>.91                       | ي<br>۱                               | 0<br>6            |
| (NH4) <sub>S</sub> SO <sub>4</sub> (AS)<br>Pooled<br>(NH4) <sub>S</sub> HPO <sub>4</sub> (DAP)<br>(NH4) <sub>S</sub> SO <sub>4</sub> (AS)<br>Pooled   | y = 294<br>y = 292<br>$y = 60_{*}^{1}$<br>$y = 20_{*}^{2}$<br>$y = 10_{*}$ | 48.7(x) + 8.05(x <sup>2</sup> ) - 0.553(x <sup>3</sup> ) + 0.0140(x <sup>4</sup> )<br>43.3(x) + 6.05(x <sup>3</sup> ) - 0.394(x <sup>3</sup> ) + 0.00948(x <sup>4</sup> )<br>- 6.06(x)<br>- 1.18(x)<br>+ 4.43(x)  | 16.<br>16.                                     | ء<br>۱                               | 6<br>6            |
| Pooled<br>(NH4) <sub>2</sub> HFO4 (DAP)<br>(NH4) <sub>2</sub> SO4 (AS)<br>Pooled  | k k × × ×  | 43.3(x) + 6.05(x <sup>2</sup> ) - 0.394(x <sup>3</sup> ) + 0.00848(x <sup>4</sup> )<br>6.06(x)<br>1.18(x)<br>+ 4.43(x)  | 16.<br>16.                                     | ۔<br>ت                               | თ<br>თ            |
| (NH4) <sub>2</sub> HFO4 (DAP)<br>(NH4) <sub>2</sub> SO4 (AS)<br>Pooled  | × × ≻<br>□ □ □   | - 6.06(x)<br>- 1.18(x)<br>+ 4.43(x)   | 16°  |                                      |                   |
| 2HPO₄ (DAP)<br>2SO₄ (AS)<br>d   | ⊨ = = =  | 6.06(x)<br>1.18(x)<br>+ 4.43(x)   | 16°  |                                      |                   |
| 2804 (AS)<br>d  | ⊨ =<br>⊨   | (x)18(x)<br>+ ۱۰٬۰۴۹(x)   | IT.  |                                      |                   |
| þd  | ≡<br>≻   | + 4.43(x)   |  |                                      |                   |
|   |  |   | . 20   | 165.4 (f = 2, 32)                    | 66                |
| Aspen excelsior fuel beds   |  |   |  |                                      |                   |
| Rate of spread (Rg) $$(\rm NH_4)_{\rm 2}HPO_4$ (DAP) 19$  | у =  | -0.332 + 6.67(x <sup>-1</sup> )   | . 97   |                                      |                   |
| $(NH_4)_{SO_4}$ (AS) 31   | ي<br>ح   | 0.330 + 5.50(x <sup>-1</sup> )  | . 87   |                                      |                   |
| Pooled 50   | ي<br>ع   | 0.147 + 5.68(x <sup>-1</sup> )  | .86  | 15.0 (f = 2, 46)                     | 66                |
| Ret# of weight loss $(R_{\rm W})$   |  |   |  |                                      |                   |
| (NH4) <sub>2</sub> HPO4 (DAP) 19  | 19 ln y = 6.19   | x ul l48.0 - 6.   | .79  |                                      |                   |
| $(NH_4) gSO_4$ (AS) 31  | 31 ln y = 5.95   | 5 - 0.295 ln x  | • 60   |                                      |                   |
| Pooled 50   | 50 ln y = 5.75   | 5 - 0.321 ln x  | . 21   | 46.7 (f = 2, 46)                     | 66                |
| Residue (R)   |  |   | •  |                                      |                   |
| $(\mathrm{NH4})_{\mathrm{S}\mathrm{HPO}_{4}}$ (DAP) 9   | 9 y = 158 + 35.0x  | 35.Ox   | 66°  |                                      |                   |
| $(NH_4)_{\mathcal{B}}SO_4$ (AS) 17  | y =  | 7.32 + 2.81x  | . 49   |                                      |                   |
| Pooled 26   | 26 y = 189 -   | 4.73x   | . 02   | 1726 (f = 2, 22)                     | 66                |

Table 3.--Regression equations for rate of spread, rate of weight loss, and residue



Figure 15.--Ponderosa pine residue for (top or bottom) untreated, 7.5 percent  $(NH_4)_2SO_4$ , and 7.5 percent  $(NH_4)_2HPO_4$  treated fuel beds.

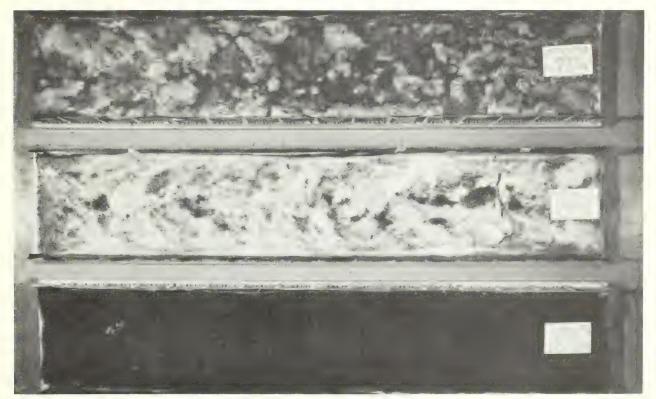


Figure 16.--Aspen excelsior residue for (top to bottom) untreated, 7.5 percent  $(NH_4)_2SO_4$ , and 7.5 percent  $(NH_4)_2HPO_4$  treated fuel beds.

# DISCUSSION

When attempting to characterize the effects of retardant chemicals on flammability, the measurement of three parameters provides a more complete picture than does the use of a single parameter. For example, the study has shown that chemicals can have similar effects on the rate of fire spread while having greatly different effects on the energy release rate and residue. Since retardant chemicals are used primarily to reduce both the combustion rate and the ability of the fire to propagate itself, it is necessary that these parameters be quantified to completely evaluate a retardant's effects on flammability.

For purposes of discussion, the effects a chemical has on flammability can be grouped under two primary considerations:

- 1. The effect the chemical has on flaming combustion, and
- 2. The effect the chemical has on glowing combustion.

Previous studies (George and Susott 1971) have indicated that the different effects ammonium phosphate and sulfate have on pyrolysis and combustion of cellulose are due to availability of the inorganic fraction involved in the reaction or to a different mechanism by which these chemicals alter pyrolysis and combustion. The results of this study indicate that although there are significant differences in the effects ammonium sulfate and phosphate have on flaming combustion, the differences in their effects on glowing combustion are much greater. It is theorized that the difference in the effects these chemicals have on glowing combustion is due to a difference in the availability of the inorganic fraction or retardant chemical. Figure 17 shows thermal decomposition curves for ammonium sulfate and ammonium phosphate.<sup>2</sup> The curves show that ammonium sulfate has completely decomposed by about 425° C. while ammonium phosphate decomposition is not complete until about 675° C. This suggests that by the time the fire has spread through an ammonium sulfate treated bed, and prior to the majority of the glowing combustion process, the ammonium sulfate may have decomposed. If this were true, the

<sup>2</sup>Figure 17 is taken from the paper by George and Susott (1971).

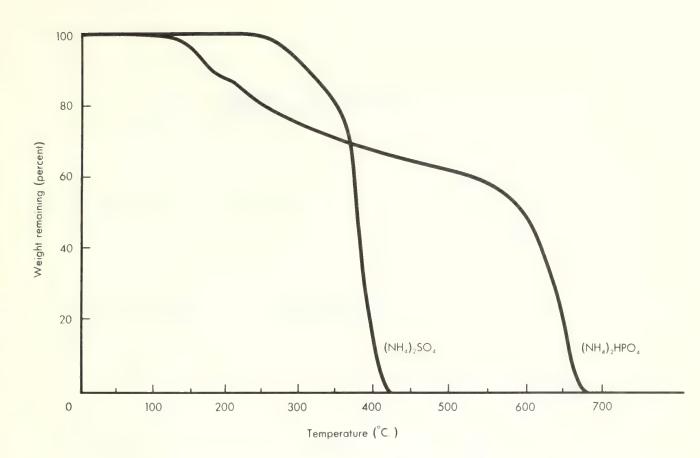


Figure 17.--Thermal decomposition curves for  $(NH_4)_2HPO_4$  and  $(NH_4)_2SO_4$  heated at 25° C./min. in a flow of 1 liter/min. air.

ammonium sulfate would affect the glowing combustion process very little. Ammonium phosphate, on the other hand, might still be present, altering glowing combustion as well as flaming combustion. This would explain why these two chemicals affect glowing combustion in different ways. This does not mean that the chemicals' effects are necessarily different because of physical degradation differences. The difference may be a chemical difference and still depend on the amount of chemical available to enter into the reaction.

Anderson (1969), using ponderosa pine needle fuel beds, similar to those of this study, found the average temperature within the combustion zone to be 867° C. Considering a reduction in these temperatures because of treatment and durational differences between temperatures measured in the combustion zone and those determined during thermal analysis, it is likely that most of the ammonium sulfate would decompose during passage of the flame front.

The effects other chemicals have on flammability can be evaluated by using the regression equations which quantify the effects of ammonium phosphate and sulfate on flammability. These relationships can be used as standards by which the effect of typical forest fire retardant additives such as thickening agents, coloring agents, and corrosion and spoilage inhibitors, can be judged.

These data can also provide the basis for linking some of the more basic pyrolysis and combustion data concerning the effects of fire retardant chemicals with actual controlled open combustion laboratory tests.

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00302, 14 p., illus.

# APPENDIX

| Fire     | : Rate of                      |                          | : Energy               | :<br>. Destilue      |
|----------|--------------------------------|--------------------------|------------------------|----------------------|
| umber    | : spread                       | 0                        | : release rate         | : Residue            |
|          | $R_{s}(ft./min.)$              | $R_{w}(g./min.)$         | E(B.t.u./min.)         | R(g.)                |
| onderos  | sa pine needle fuel            | beds                     |                        |                      |
| 1-PP     | 1.70                           | 291                      | 5,610                  |                      |
| 2-PP     | 1.71                           | 330                      | 6,362                  |                      |
| 3-PP     | 1.77                           | 276                      | 5,321                  |                      |
| 4–PP     | 1.81                           | 299                      | 5,765                  |                      |
| 5-PP     | 1.70                           | 290                      | 5,591                  |                      |
| 6-PP     | 1.75                           | 257                      | 4,955                  |                      |
| 7-PP     | 2.02                           | 296                      | 5,707                  | 321                  |
| 8-PP     | 1.85                           | 290                      | 5,591                  | 295                  |
| 9-PP     | 1.89                           | 315                      | 6,073                  | 300                  |
| 0-PP     | 1.92                           |                          |                        | 315                  |
| 1-PP     | 1.89                           | 299                      | 5,765                  | 285                  |
| 2-PP     | 1.68                           | 290                      | 5,591                  |                      |
|          |                                |                          |                        |                      |
|          | $\overline{R}_{s} = 1.81$      | $\overline{R}_{W} = 294$ | $\overline{E} = 5,668$ | $\overline{R} = 303$ |
|          | $S_{m} \frac{1}{2} = \pm 0.03$ | $S_m = \pm 3.3$          | $S_m = \pm 64$         | $S_m = \pm 6.6$      |
| spen exc | celsior fuel beds              |                          |                        |                      |
| 1-E      | 4.44                           | 462                      | 8,635                  | 0                    |
| 2-E      | 3.51                           | 474                      | 8,859                  | 0                    |
| 3-E      | 3.70                           | 467                      | 8,728                  | 0                    |
| 4–E      | 4.31                           | 463                      | 8,653                  | 0                    |
| 5-E      | 4.44                           | 450                      | 8,411                  | 0                    |
| 6-E      | 3.70                           | 486                      | 9,083                  | 0                    |
| 7-E      | 4.71                           | 441                      | 8,242                  | 0                    |
| 8-E      | 3.74                           | 424                      | 7,925                  | 2                    |
| 9-E      | 3.81                           | 462                      | 8,635                  | 20                   |
|          |                                |                          | ,                      |                      |
|          | $\overline{R}_{s} = 4.04$      | $\overline{R}_{W} = 459$ | $\overline{E} = 8,579$ | $\overline{R} = 2$   |
|          | $S_{m} = \pm 0.14$             | $S_m \approx \pm 6.1$    | $S_{m} = \pm 114$      | S <sub>m</sub> = 0   |
|          | m                              | m                        | m                      | m                    |

| Table 4Summary | of test  | data f  | for | untreated | ponderosa | pine | needle |
|----------------|----------|---------|-----|-----------|-----------|------|--------|
| and aspe       | en excel | sior fi | uel | beds      |           |      |        |

 $\frac{1}{S_m}$  = standard error of the mean (S<sub>m</sub> = standard deviation/ $\sqrt{n}$ .)

| Residue              |  |               |       |       |       | 0 0.0 |       | 96.7  |               |               |       |       |       |       | 112.0 |       |               |        | 0.011 0 |       | 128.3 |        | 128.3 |        | 120.0  |        |                |        | 156.7  |                |        | 161.7  |  |
|----------------------|--|---------------|-------|-------|-------|-------|-------|-------|---------------|---------------|-------|-------|-------|-------|-------|-------|---------------|--------|---------|-------|-------|--------|-------|--------|--------|--------|----------------|--------|--------|----------------|--------|--------|--|
| 80                   | Grems                                      |               |       |       |       | 510   |       | 560   | 54C           | 565           | 530   |       |       |       | 635   |       |               |        | 630     |       | 685   | 630    | 685   |        | 660    | 730    | 725            |        | 770    | 760            | 644    | 785    |  |
| Fire characteristics | Energy<br>release rate                     | E(B.t.u./min. | 4.299 | 4,492 | 3,895 | 3,779 | 3.952 | 3,085 | 3,258         | 3,548         | 3,682 | 3.470 | 3,162 | 3,856 | 3,278 | 3,143 | 3,355         | 3,104  | 3,779   | 2,526 | 2,834 | 2,140  | 1.523 | 1,485  | 2,641  | 2,487  | 1,947          | 1,369  | 1,812  | 1,870          | 1 ,523 | 1,465  |  |
| J.L.                 | Rate of<br>weight loss                     | Rw(g./min.)   | 223   | 233   | 202   | 196   | 205   | 160   | 169           | 184           | 161   | 180   | 164   | 200   | 170   | 163   | 174           | 161    | 196     | 131   | 147   | 111    | 79    | 77     | 137    | 129    | TOT            | 71     | 94     | 97             | 79     | 76     |  |
|                      | Rate of<br>spread                          | Rg(ft./min.)  | 1.46  | 1.68  | 1.55  | 1.70  | 1.53  | 1.27  | 1.08          | 1.26          | 1.39  | 1.36  | 1.21  | 1.25  | 0.93  | 0.82  | 0.69          | 0.75   | 0.94    | 0, 69 | 0.70  | 0.43   | 0.33  | 0,28   | 0.68   | 0.50   | 0.35           | 0,26   | 0.37   | 0.39           | 0.38   | 0.33   |  |
|                      | Dry fuel<br>weight                         | Percent       | 0.97  | 0.96  | 0.95  | 66°0  | 2,05  | 1.98  | 1.96          | 1 <b>.</b> 99 | 1.94  | 80°8  | 3.00  | 2.90  | 3°05  | 4°05  | 3 <b>.</b> 95 | 4.19   | 4°00    | 5°01  | 4°79  | 5.21   | 4°99  | 6,10   | 5°71   | 5°95   | 5,90           | 7.29   | 6.80   | 7.05           | 7.11   | 7.98   |  |
| Chemical applied     | Anhydrous<br>chemical/ft. <sup>3</sup>     | Grams/ft.a    | 2,03  | 2.01  | 1.99  | 2°08  | 4.31  | 4.15  | 4.12          | 4.17          | 4。08  | 6.25  | 6,31  | 6°03  | 6.41  | 8.50  | 8.29          | 8.79   | 8.42    | 10.52 | 10.05 | 10,94  | 10.47 | 12,81  |        | 12.50  | 12,38          | 15.31  | 14.29  | 14.80          | 14.94  | 16.75  |  |
| Chemica              | Anhydrous<br>chemical                      | Grams         | 24.4  | 24.1  | 23.9  | 25.0  | 51.8  | 49.8  | 49 <b>.</b> 5 | 50°0          | 49°O  | 75.0  | 75.8  | 73°1  | 76.9  | 102.0 | 99 <b>°</b> 5 | 105.5  | 101.0   | 126.2 | 120.6 | 131.2  | 125.6 | 153.8  | 144.0  | 150°0  | 148 <b>.</b> 5 | 183.8  | 171.5  | 177 <b>.</b> 6 | 179.4  | 201.0  |  |
|                      | Bolution                                   | Grams         | 975   | 965   | 955   | 1,000 | 1,035 |       | 066           | 1,000         | 980   | 1,000 | 1,010 | 975   | 1,025 | 1,020 | 995           | 1,055  | 1,010   | 1.010 | 965   | 1,050  |       | 1,025  | 960    | 1,000  | 066            | 1,050  |        | 1,015          |        | 1,005  |  |
|                      | Treatment solution<br>(chemical by weight) | Percent       | 2.5   | 2°2   | 2.5   | 2.5   | 5.0   | 5.0   | 5.0           | 5.0           | 5°0   | 7.5   | 7.5   | 7.5   | 7.5   | 10.0  | 10.0          | 10.0   | 10.0    | 12,5  | 12.5  | 12.5   | 12.5  | 15.0   | 15.0   | 15.0   | 15.0           | 17.5   | 17.5   | 17.5           | 17.5   | 20.0   |  |
|                      | Fire number                                |               |       | 2.5 B |       |       |       |       |               | 5.0 D         |       |       | 7.5 B |       |       |       |               | 10°0 C |         |       |       | 12.5 C |       | 15.0 A | 15.0 B | 15.0 C |                | 17.5 A | 17.5 B | 17.5 C         |        | 20°0 A |  |

Table 5.--Summary of test data for  $({\it NH}_4)_2{\it HPO}_4$  treated ponderosa pine needle fuel beds

|                      | Residue          | Percent increase<br>over untreated         |                          |        |       |       | 13.3         |               | 36.7  | 6.7  | 50.0    |       | 68.3    | 47.3  | 30.3  |       |       |        | 31.7  |       | 55.0   | 28.3   | 40.7  |        |       | 56.0    |        | 62.3  | 27.0   | 32.0    |  |
|----------------------|------------------|--|--------------------------|--------|-------|-------|--------------|---------------|-------|------|---------|-------|---------|-------|-------|-------|-------|--------|-------|-------|--------|--------|-------|--------|-------|---------|--------|-------|--------|---------|--|
|                      | Rea              | Grams ove                                  |                          |        |       |       | 340          |               | 410   | 320  | 450     |       | 505     | 442   | 391   |       |       |        | 395   |       | 465    | 385    | 422   |        |       | 468     |        | 487   | 381    | 395     |  |
| Fire characteristics |                  | Energy<br>release rate Gr                  | E(B.t.u./min.)           | 4.184  | 4.396 | 4.338 |              | 4,203         |       |      | 3,779 4 | 4,087 | 3,046 5 |       |       | 4,049 | 3,451 | 3,760  |       | 3,220 |        |        |       | 2,275  | 2,911 | 2,757 4 | 3,008  |       |        | 2,198 3 |  |
| Fire                 |                  | Rate of<br>weight loss                     | R <sub>w</sub> (g./min.) | 217    | 228   | 225   | 217          | 218           | 198   | 170  | 196     | 212   | 158     | 162   | 180   | 210   | 179   | 195    | 143   | . 167 | 156    | 197    | 165   | 118    | 151   | 143     | 156    | 113   | 135    | 114     |  |
|                      |                  | Rate<br>spread                             | • Rg(ft./min.)           | 1.52   | 1.50  | 1.52  | 1.76         | 1.31          | 1.18  | 1.32 | 1.68    | 1.36  | 1.05    | 1.06  | 1.22  | 0.92  | 0°*0  | 0.98   | 1.03  | 0°75  | 0.72   | 0.89   | 0.90  | 0.56   | 0.52  | 0.54    | 0.56   | 0.43  | 0.45   | 0。44    |  |
|                      |                  | Dry fuel<br>weight                         | Percent                  | 1,04   | .96   | .98   | 66*          | 2.01          | 1.96  | 1.91 | 1.92    | 2.89  | 2.92    | 2.98  | 3.11  | 4.09  | 3.91  | 4.15   | 4.07  | 4.96  | 4.73   | 4.59   | 4.99  | 5.70   | 6.07  | 5,92    | 7.09   | 6.40  | 7.21   | 8.36    |  |
|                      | Chemical applied | Anhydrous<br>chemical/ft. <sup>2</sup>     | Grams/ft. <sup>2</sup>   | 2,19   | 2.02  | 2.05  | 2°07         | 4.23          | 4.11  | 4.02 | 4°03    | 6.06  | 6.13    | 6.25  | 6.53  | 8.58  | 8.21  | 8.71   | 8。54  | 10.42 | 9.93   | 9.64   | 10.47 | 11.98  | 12.75 | 12.44   | 14.88  | 13.45 | 15.15  | 17.55   |  |
|                      | Chemice.         | Anhydrous<br>ohemicel                      | Grams                    | 26.3   | 24.3  | 24.6  | 24.8         | 50 <b>.</b> 8 | 49.3  | 48.3 | 48.4    | 72.8  | 73.5    | 75.0  | 78.4  | 103.0 | 98°5  | 104.5  | 102.5 | 125.0 | 119.1  | 115.6  | 125.6 | 143.7  | 153.O | 149°3   | 178.5  | 161.4 | 181.8  | 210.6   |  |
|                      |                  | Solution                                   | Grems                    | 1,050  | 970   | 985   | 995          | 1,015         | 986   | 965  | 968     | 970   | 980     | 1,000 | 1,045 | 1,030 | 985   | 1,045  | 1,025 | 1,000 | 953    | 925    | 1,005 | 958    | 1,020 | 395     | 1,020  | 922   | 1,039  | 1,053   |  |
|                      |                  | Treatment solution<br>(chemical by weight) | Percent                  | ິ<br>ເ | 2.5   | 2°2   | ວ <b>ໍ</b> ຄ | 5.0           | 5.0   | 5.0  | 5.0     | 7.5   | 7.5     | 7°5   | 7.5   | 10.0  | 10.0  | 10.0   | 10.0  | 12.5  | 12.5   | 12.5   | 12.5  | 15.0   | 15.0  | 15.0    | 17.5   | 17.5  | 17.5   | 20.0    |  |
|                      |                  | Fire number                                |                          | ß      | 2.5 B | ß     | ß            |               | 5.0 B | 0    | 5.0 D   |       |         | 7.5 C |       |       |       | 10°0 C |       |       | 12.5 B | 12.5 C | ß     | 15.0 A |       |         | 17.5 A |       | 17.5 C | 20°0 A  |  |

Table 6.--Summary of test data for  $({\rm NH}_{4})_2{\rm SO}_4$  treated ponderosa pine fuel beds

Table 7.--Summary of test data for  $({\rm NH}_{\rm H})_{2\rm HPO}_{\rm H}$  treated aspen excelsior fuel beds

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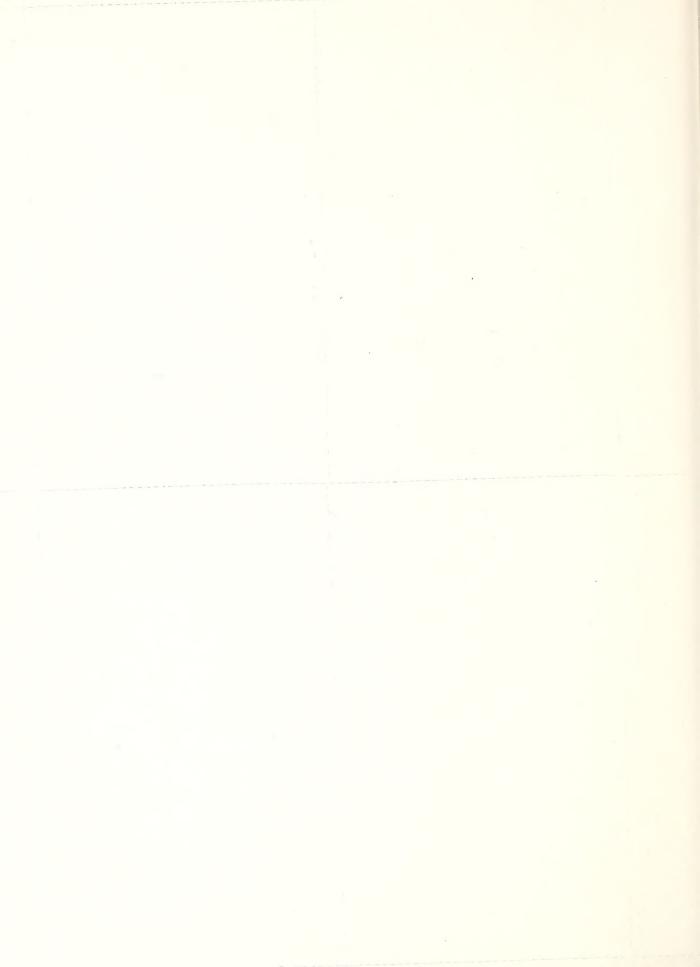
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| Grams<br>Grams<br>15<br>15<br>65<br>28<br>28<br>28<br>28<br>28<br>28<br>28<br>28<br>28<br>28<br>28<br>28<br>25<br>55<br>55<br>55<br>55<br>55<br>55<br>55<br>55<br>55<br>55<br>55<br>55  |             |            |            |                       |                        |                    |                   | 2.7T.J                 | FIFE CDEFECTORISTICS   | 20       |                                    |
|---|-------------|------------|------------|-----------------------|------------------------|--------------------|-------------------|------------------------|------------------------|----------|------------------------------------|
|   |             |            |            | Chemica               | l applied              |                    |                   |                        |                        |          | Residue                            |
| Percent         Greand         Greand $T_{eff}$ Percent $T_{eff}$ $T_{efff}$ $T_{efff}$ $T_{e$  | Fire number |            | Solution   | Anhydrous<br>chemical |                        | Dry fuel<br>weight | Rete of<br>spread | Rate of<br>weight loss | Energy<br>release rate | Grams    | Percent increase<br>over untreated |
|   |             |            | Grams      | Grams                 | Grams/ft. <sup>2</sup> | Percent            | Rg(ft./min.)      | Rw(g./min.)            | E(B.t.u./min.)         |          |                                    |
|   | ß           | ວ° ບ       | 395        | 24.9                  | 2.07                   | 1.47               | 3.78              | 340                    | 6.355                  |          |                                    |
|   | ŝ           | 2.5        | 960        | 24.0                  | 2.00                   | 1.42               | 2.94              | 352                    | 6,579                  |          |                                    |
|   | ŝ           | ວູ<br>ເ    | 940        | 23 5                  | 1.96                   | 1.39               | 3.48              | 296                    | 5,532                  |          |                                    |
| $Z_{1,0}$ $Y_{1,0}$ $Z_{1,4}$ $Z_{1,0}$ $Y_{1,0}$ $Z_{1,1}$ $Z_{1,0}$ $Z_{1,1}$ $Z_{1,2}$ $Z_{1,1}$ <   | ഹ           | ະນີ<br>ເ   | 1,035      | 25.9                  | 2.16                   | 1.53               | 2.56              | 307                    | 5,738                  | ŝ        | 5                                  |
|   | ß           | 2.5        | 975        | 24.4                  | 2°03                   | 1。44               | 2.78              | 3,23                   | 6,037                  | 30       | 30                                 |
|   |             | 5.0        | 010-1      | 50.5                  | 14.27                  | 66.4               | 2.03              | 203                    | 5 476                  |          |                                    |
|   |             | 5.0        | 985        | 49.3                  | 4.10                   | 16.2               | 1.04              | 233                    | 4 355                  | 5        | 15                                 |
|   |             | 5.0        | 950        | 47.5                  | 3.96                   | 2.81               | 2.08              | 321                    | 5,999                  |          |                                    |
| 7.5 $7.6$ $995$ $74.6$ $6.23$ $4.41$ $1.02$ $217$ $5.944$ $23$ $7.5$ $1.000$ $75.6$ $6.23$ $4.43$ $0.084$ $110$ $3.777$ $23$ $7.5$ $1.000$ $75.6$ $6.23$ $4.43$ $0.084$ $100$ $3.774$ $23$ $110.0$ $1.000$ $1060$ $106.0$ $8.83$ $6.291$ $0.08$ $100$ $3.774$ $23$ $110.0$ $1.000$ $1060$ $106.0$ $8.83$ $6.291$ $100$ $3.774$ $23$ $110.0$ $1.000$ $106.0$ $8.83$ $6.291$ $1.00$ $3.774$ $23$ $110.0$ $1.000$ $106.0$ $8.83$ $6.291$ $1.10$ $3.742$ $5.742$ $5.742$ $112.5$ $1.000$ $132.5$ $11.03$ $7.43$ $0.296$ $1.72$ $2.742$ $2.742$ $5.742$ $5.742$ $5.742$ $5.742$ $5.742$ <t< td=""><td></td><td>5.0</td><td>046</td><td>48.5</td><td>4.04</td><td>2.87</td><td>1.10</td><td>222</td><td>4,149</td><td>5</td><td><u>م</u> (</td></t<>  |             | 5.0        | 046        | 48.5                  | 4.04                   | 2.87               | 1.10              | 222                    | 4,149                  | 5        | <u>م</u> (                         |
| $ \begin{array}{cccccccccccccccccccccccccccccccccccc$   |             | 7.5        | 995        | 74.6                  | 22                     | 4.47               | 30 L              | רוט                    | 2 944                  |          |                                    |
|   |             | 7.5        | 000. [     | 75.0                  | 6.25                   | 4.43               | 0.84              | 170                    | 2177                   | 28       | 98                                 |
|   |             | 5 5        | 2001       | 75.4                  | 6 98<br>8              | 1 15               | 40°0              |                        | 2 264                  | 002      |                                    |
| $N_{10}$ $V_{10}$   |             | о и<br>- с | ,          | * ° C - *             | 02.0                   | 4°40               | 00.00             | 001                    | 400°°0                 | 00       | 00                                 |
| A         10.0         1,060         106.0         8.83         6.26         0.84         182         3,402           D         10.0         1,000         100.0         8.83         6.26         1,210         204         3,813           D         10.0         1,000         100.0         8.83         6.26         1,210         204         3,813           D         10.0         1,000         105.0         8.85         6.09         1,210         204         3,813           D         12.5         1,000         135.5         11.04         7.85         0.67         167         3,046         55           D         12.5         1,000         135.6         11.26         7.45         0.67         177         4,616         15           D         12.5         1,000         135.6         11.26         7.45         0.67         177         3,204         55           D         12.5         1,000         126.0         10.51         7.45         0.67         177         3,204         56           D         12.5         12.50         12.51         12.51         12.51         2.341         2.52         2.414         2.52 <td></td> <td>G * J.</td> <td>200<br/>200</td> <td>C°cJ.</td> <td>CT°Q</td> <td>4.00</td> <td>U. 88</td> <td>TAB</td> <td>\$10°C</td> <td></td> <td></td> |             | G * J.     | 200<br>200 | C°cJ.                 | CT°Q                   | 4.00               | U. 88             | TAB                    | \$10°C                 |          |                                    |
| B         10.0         1,000         100.0         10.0         1,000         100.0         8.33         5.91         0.98         204         5,813           C         10.0         1,060         106.0         8.58         6.09         1.10         219         4,033         15           B         12.5         1,060         132.5         11.04         7.83         0.67         177         4,033         16         15         17         4,033         15         15         10.03         125.0         11.04         7.83         0.67         177         5,013         65         12         167         3,046         65         12         12         177         5,013         177         5,712         22         12         12         177         5,712         22         12         12         177         5,712         22         12         12         177         5,712         22         12         12         1177         5,712         22         12         12         12         12         12         12         12         12         12         12         12         12         12         12         12         12         12         12  |             | 10.0       | 1,060      | 106.0                 | 8.83                   | 6.26               | 0.84              | 182                    | 3.402                  |          |                                    |
| $ \begin{array}{cccccccccccccccccccccccccccccccccccc$   |             | 10.0       | 1,000      | 100.0                 | 8,33                   | 5.91               | 0.98              | 204                    | 3,813                  |          |                                    |
| $ \begin{array}{cccccccccccccccccccccccccccccccccccc$   |             | 10.0       | 1,030      | 103.0                 | 8.58                   | 6,09               | 1.10              | 219                    | 4,093                  |          |                                    |
| A         12.5         1,060         132.5         11.04         7.98         0.67         163         5,046         65           C         12.5         1,080         135.0         11.25         1.080         135.0         11.25         5,046         65           C         12.5         990         125.6         10.51         7.98         0.67         167         3,212         25           A         15.0         985         147.8         12.31         7.45         0.67         167         3,121         25           A         15.0         985         147.8         12.31         7.31         0.72         157         3,731         25           C         15.0         990         148.5         12.13         8.60         1.11         21         25           D         15.0         990         145.5         12.13         8.60         1.11         218         204           D         15.0         990         1445.5         12.13         8.60         1.11         218         200         28         214         20           D         15.0         985         12.38         8.78         0.68         200  |             | 10.0       | 1,060      | 106.0                 | 8.83                   | 6.26               | 1.21              | 247                    | 4,616                  | 15       | 15                                 |
| B         12.5         1,080         135.0         11.25         7,98         0.90         177         5,308         65           C         12.5         1,008         125.0         10.31         7,31         0.87         177         5,308         65           A         15.0         985         147.8         12.51         10.51         7.31         0.87         177         5,308         65           A         15.0         985         147.8         12.31         7.31         0.72         157         3,121         22           B         15.0         995         145.5         12.31         7.31         0.72         222         4,149           C         15.0         995         148.5         12.38         8.60         1.11         218         4,074           D         15.0         996         172.4         14.36         12.38         8.778         0.66         4,074           D         15.0         177.5         12.36         0.66         1.11         22         28         27         4         77           D         15.0         12.36         0.65         12.48         0.68         200         27  |             | 12.5       | 090.1      | 132.5                 | 40 - LT                | 7,83               | 0.67              | 29 L                   | 3 046                  |          |                                    |
| $ \begin{array}{cccccccccccccccccccccccccccccccccccc$   |             | 5          | URO L      | 135.0                 | 25 11                  | 7 98               | 0 90              | 242 L                  | 3 308                  | A F      | 3                                  |
| D         12.5         1,008         126.0         10.50         7.45         0.67         167         5,121         22           B         15.0         985         147.8         12.31         7.45         0.67         167         5,121         22           B         15.0         985         147.8         12.31         7.31         0.72         152         2,841           C         15.0         970         148.5         12.15         9.04         0.95         22.8         4,149           C         15.0         990         148.5         12.13         8.60         1.11         218         4,074           D         15.0         990         148.5         12.38         8.60         1.11         218         4,074           D         17.5         985         179.4         14.36         10.61         0.65         2,355         28           A         17.5         1,026         179.6         14,96         10.61         0.65         2,355         28           B         20.0         177.5         14,96         0.61         0.65         2,355         28           C         17.5         14,96         0   |             |            | 066        | 123.8                 | 10.31                  | 12.7               | 0.87              | 175                    | 3 271                  | 200      | 300                                |
| A         15.0         985         147.8         12.31         7.31         0.72         152         2,841           B         15.0         17.020         153.0         12.15         9.04         0.95         222         4,149           C         15.0         970         148.5         12.15         9.04         0.95         222         4,149           C         15.0         970         148.5         12.15         9.06         1.11         218         4,074           D         15.0         990         148.5         12.13         8.60         1.11         218         4,074           A         17.5         985         17.46         14.36         10.61         0.65         2,356         28           A         17.5         1,026         179.6         14,96         10.61         0.65         2,356         28           B         20.0         1,7.6         14,96         10.61         0.65         2,719         56           B         20.0         1,060         20.0         12.41         0.66         3,736         56           B         20.0         10.61         0.65         114.96         0.65  |             | 12.5       | 1,008      | 126.0                 | 10.50                  | 7.45               | 0.67              | 167                    | 3,121                  | 22       | 22                                 |
| B         15.0         1,020         155.0         12.75         9.04         0.95         222         4,074           D         15.0         970         145.5         12.75         9.04         0.95         222         4,074           D         15.0         990         148.5         12.75         8.60         1.11         218         4,074           A         17.5         985         172.4         14.36         10.18         1.09         260         4,859           B         17.5         1,028         179.9         14.95         10.61         0.65         1255         28           C         17.5         1,026         179.6         14.96         10.61         0.62         255         28           A         20.0         1,026         179.6         14.96         10.61         0.62         27,719         56           B         20.0         1,050         210.0         17.49         11.496         0.66         3,7719         56           B         20.0         10.61         0.66         1356         3,739         56           B         20.0         11.48         0.66         156         55   |             | 15.0       | 985        | 147.8                 | 12.31                  | 7.31               | 0.72              | 152                    | 2.841                  |          |                                    |
| 0         15.0         970         145.5         12.13         8.60         1.11         218         4.074           0         15.0         990         148.5         12.13         8.60         1.11         218         4.074           A         17.5         985         172.4         14.36         10.18         1.09         260         4.859         40           B         17.5         1,028         179.9         14.96         10.63         0.055         2.336         28           C         17.5         1,026         179.6         14.96         10.61         0.62         125         2.335         28           A         20.0         17.65         14.96         10.61         0.62         135         2.523         65           B         20.0         10.61         16.75         11.88         0.96         3.738         55           B         20.0         980         196.0         16.75         11.88         0.96         3.738         55  |             | 15.0       | 1.020      | 153.0                 | 12.75                  | 9.04               | 0.95              | 222                    | 4.149                  |          |                                    |
| D         15.0         990         148.5         12.38         8.78         0.88         200         3,738         40           A         17.5         985         17.4         14.36         10.18         1.09         260         3,738         40           B         17.5         1,028         179.4         14.36         10.61         0.65         126         4,659         28           C         17.5         1,026         179.6         14.96         10.61         0.62         1355         2,535         28           A         20.0         1,050         210.0         17.50         12.41         0.66         1355         2,533         65           B         20.0         10,050         201.0         16.75         11.48         0.66         1355         2,533         65           B         20.0         980         196.0         16.75         11.48         0.46         3,738         55  |             | 15.0       | 970        | 145.5                 | 12.13                  | 8.60               | 11.1              | 218                    | 4.074                  |          |                                    |
| A         17.5         985         172.4         14.36         10.18         1.09         260         4.659           B         17.5         1,028         179.9         14.96         10.63         0.55         125         2.336         28           C         17.5         1,026         179.6         14.96         10.61         0.62         199         3.719         56           A         20.0         1,050         210.0         17.50         12.41         0.66         135         2.523         65           B         20.0         1,050         20.0         16.75         11.88         0.92         190         3.736         55           C         0.05         20.0         16.75         11.88         0.92         190         3.738         55  |             | 15.0       | 066        | 148.5                 | 12.38                  | 8.78               | 0.88              | 200                    | 3,738                  | 40       | 40                                 |
| B         17.5         1,028         179.9         14.99         10.63         0.55         125         2,336         28           C         17.5         1,026         179.6         14.96         10.61         0.62         125         2,336         28           A         20.0         1,026         210.0         14.96         10.61         0.62         139         3,719         56           B         20.0         1,050         210.0         17.50         12.41         0.66         135         2,523         65           B         20.0         1,005         201.0         16.75         11.88         0.922         190         3,551         57           C         20.0         980         196.0         16.73         11.58         0.88         200         3,738         55  |             | 17.5       | 985        | 172.4                 | 14.36                  | 10.18              | 1,09              | 260                    | 4.859                  |          |                                    |
| C         17.5         1.026         179.6         14.96         10.61         0.62         199         3,719         56           A         20.0         1,050         210.0         17.50         14.96         10.61         0.62         139         3,719         56           B         20.0         1,050         210.0         17.50         12.41         0.66         135         2,523         65           B         20.0         1,005         201.0         16.75         11.88         0.92         190         3,551         57           C         20.0         980         196.0         16.33         11.58         0.88         200         3,738         55  |             | 17.5       | 1,028      | 179.9                 | 14.99                  | 10.63              | 0.55              | 125                    | 2 336                  | ac<br>ac | 80                                 |
| A     20.0     1,050     210.0     17.50     12.41     0.66     135     2,523     65       B     20.0     1,005     201.0     16.75     11.68     0.92     190     3,551     57       C     20.0     15.05     201.0     16.33     11.58     0.88     200     3,738     55  |             | 17.5       | 1,026      | 179.6                 | 14.96                  | 10.61              | 0.62              | 199                    | 3,719                  | 56       | 56                                 |
| A         20.0         1,050         210.0         17.50         12.41         0.66         135         2,523         65           B         20.0         1,005         201.0         16.75         11.88         0.92         190         3,551         57           C         20.0         1,005         201.0         16.75         11.58         0.92         190         3,551         57           C         20.0         980         196.0         16.33         11.58         0.88         200         3,738         55   |             |            |            |                       |                        |                    |                   |                        |                        |          |                                    |
| B 20.0 1,005 201.0 16.75 11.88 0.92 190 3,551 57<br>C 20.0 980 196.0 16.33 11.58 0.88 200 3,738 55  |             | 20.0       | 1,050      | 210°0                 | 17.50                  | 12.41              | 0.66              | 135                    | 2,523                  | 65       | 65                                 |
| 0 20.0 980 196.0 16.33 11.58 0.88 200 3.738 55  |             | 20.0       | 1,005      | 201.0                 | 16.75                  | 11.88              | 0.92              | 190                    | 3,551                  | 57       | 57                                 |
|   |             | 20°0       | 980        | 196°O                 | 16 <b>.</b> 33         | 11.58              | 0.88              | 200                    | 3,738                  | 55       | 55                                 |

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| <ul> <li>GEORGE, CHARLES W., and AYLMER D. BLAKELY</li> <li>1972. Effects of ammonium sulfate and ammonium phosphate on flammability USDA Forest Serv. Res. Pap. INT-121, 26 p., illus. Intermountain Forest and Range Exp. Sta., Ogden, Utah 84401.</li> <li>Pine needle and excelsior fuel beds treated with various amounts of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>HPO<sub>4</sub> were burned in an environmentally controlled wind tunnel. The two chemicals have different effects on the rate of fire spread, rate of weight loss or equivalent energy release rate, residue, and thus on flammability. The differences these chemicals have on glowing combustion phase are probably due to the difference in their thermal behavior and hence availability.</li> </ul>  | <ul> <li>GEORGE, CHARLES W., and AYLMER D. BLAKELY</li> <li>1972. Effects of ammonium sulfate and ammonium phosphate on flammability. USDA Forest Serv. Res. Pap. INT-121, 26 p., illus. Intermountain Forest and Range Exp. Sta., Ogden, Utah 84401.</li> <li>Pine needle and excelsior fuel beds treated with various amounts of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>HPO<sub>4</sub> were burned in an environmentally controlled wind tunnel. The two chemicals have different effects on the rate of fire spread, rate of weight loss or equivalent energy release rate, residue, and thus on flammability. The differences these chemicals have on glowing combustion phase are probably due to the difference in their thermal behavior and hence availability.</li> </ul> |
|---|---|
| <ul> <li>GEORGE, CHARLES W., and AYLMER D. BLAKELY</li> <li>1972. Effects of ammonium sulfate and ammonium phosphate on flammability. USDA Forest Serv. Res. Pap. INT-121, 26 p., illus. Intermountain Forest and Range Exp. Sta., Ogden, Utah 84401.</li> <li>Pine needle and excelsior fuel beds treated with various amounts of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>HPO<sub>4</sub> were burned in an environmentally controlled wind tunnel. The two chemicals have different effects on the rate of fire spread, rate of weight loss or equivalent energy release rate, residue, and thus on flammability. The differences these chemicals have on glowing combustion phase are probably due to the difference in their thermal behavior and hence availability.</li> </ul> | <ul> <li>GEORGE, CHARLES W., and AYLMER D. BLAKELY</li> <li>1972. Effects of ammonium sulfate and ammonium phosphate on flammability. USDA Forest Serv. Res. Pap. INT-121, 26 p., illus. Intermountain Forest and Range Exp. Sta., Ogden, Utah 84401.</li> <li>Pine needle and excelsior fuel beds treated with various amounts of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>HPO<sub>4</sub> were burned in an environmentally controlled wind tunnel. The two chemicals have different effects on the rate of fire spread, rate of weight loss or equivalent energy release rate, residue, and thus on flammability. The differences these chemicals have on glowing combustion phase are probably due to the difference in their thermal behavior and hence availability.</li> </ul> |



Headquarters for the Intermountain Forest and Range Experiment Station are in Ogden, Utah. Field Research Work Units are maintained in:

Boise, Idaho

Bozeman, Montana (in cooperation with Montana State University)

Logan, Utah (in cooperation with Utah State University)

Missoula, Montana (in cooperation with University of Montana)

Moscow, Idaho (in cooperation with the University of Idaho)

Provo, Utah (in cooperation with Brigham Young University)

